

Steady-state, simultaneous two-phase flow in porous media: An experimental study

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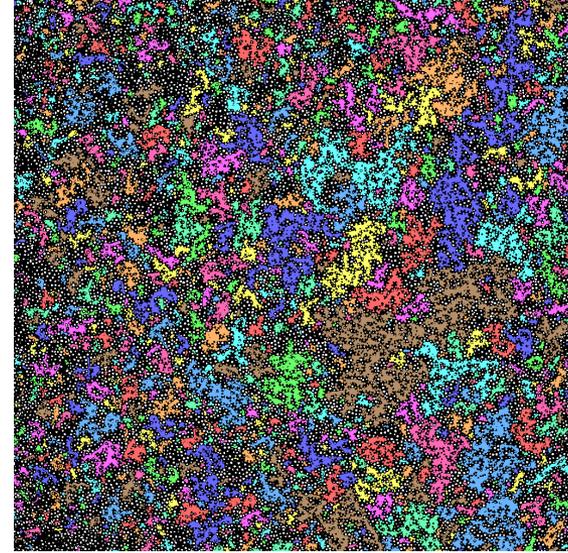
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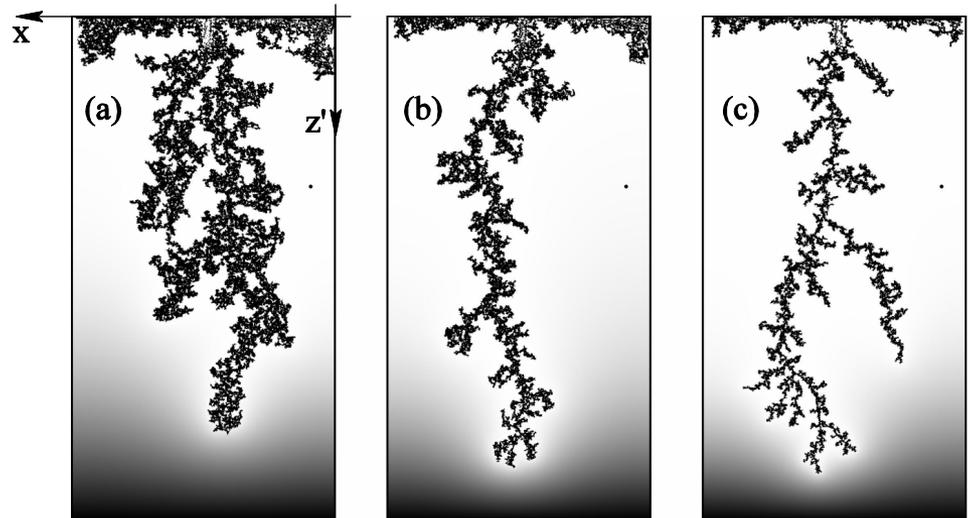
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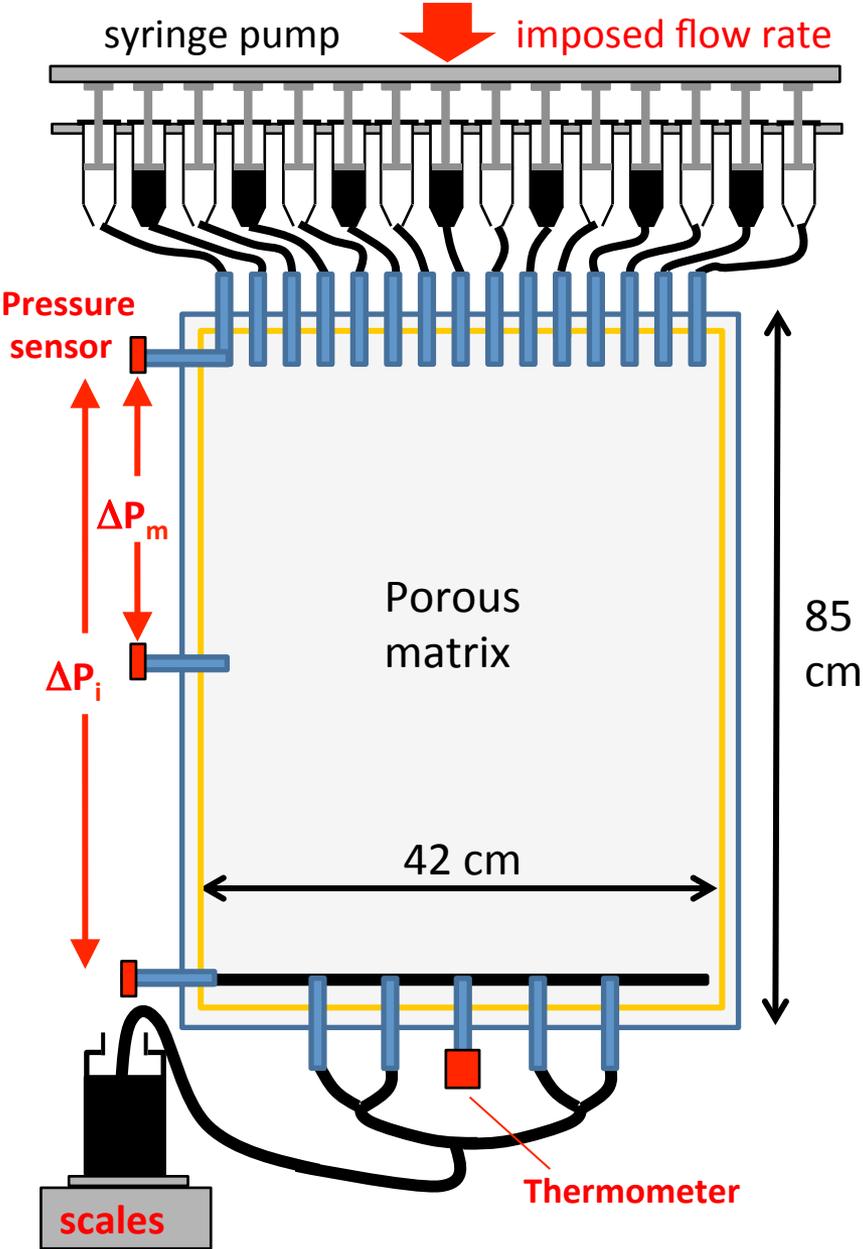
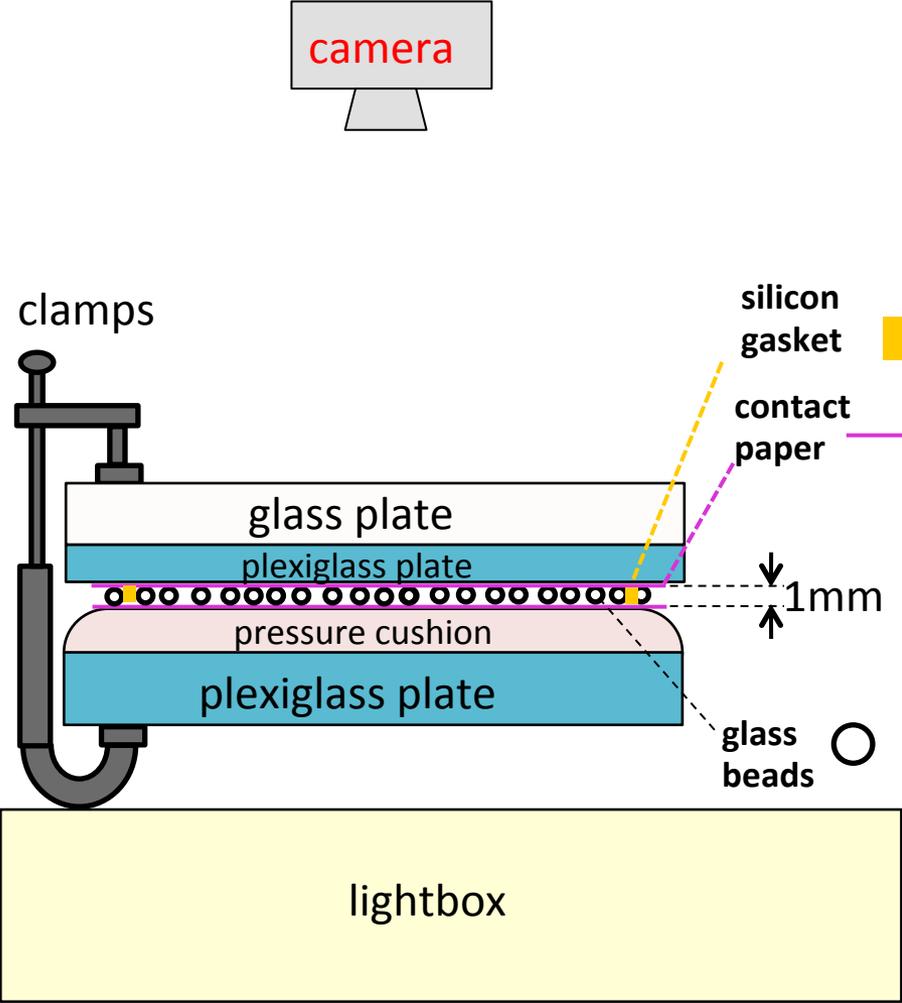
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Experimental setup



Simultaneous injection of two fluids.

Will discuss two cases:

A) Non wetting fluid: Air Wetting fluid: Water-glycerol (15% water b.w.)
Viscosity contrast 10^{-4} , Surface tension $0,064 \text{ Nm}^{-1}$

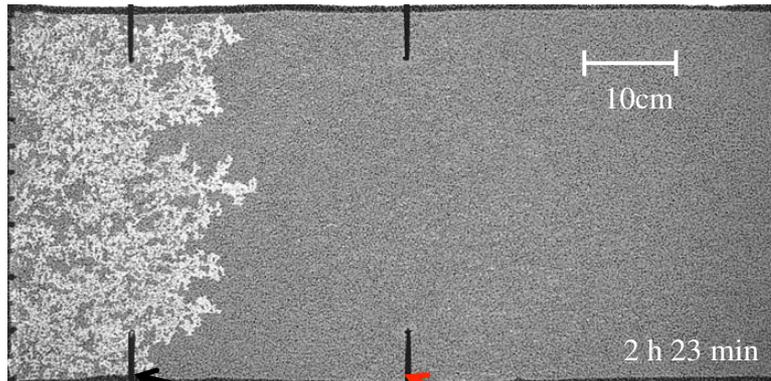
B) Non wetting fluid: Rapeseed Oil Wetting fluid: Water-glycerol (20%water b.w.)
Viscosity contrast 1.3, Surface tension $0,019 \text{ Nm}^{-1}$

Case A)

Non wetting fluid: Air

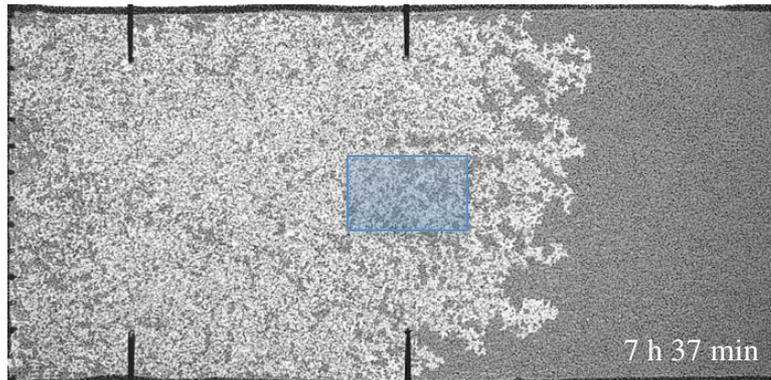
Wetting fluid: Water-glycerol

Front propagation



(a)

Pressure sensors



(b)

Transient regime

$$Ca = \frac{\mu_w Q_w a^2}{\gamma \kappa_0 A}$$

$$Ca = 0.0079$$

Dynamic cluster configuration

Steady state regime



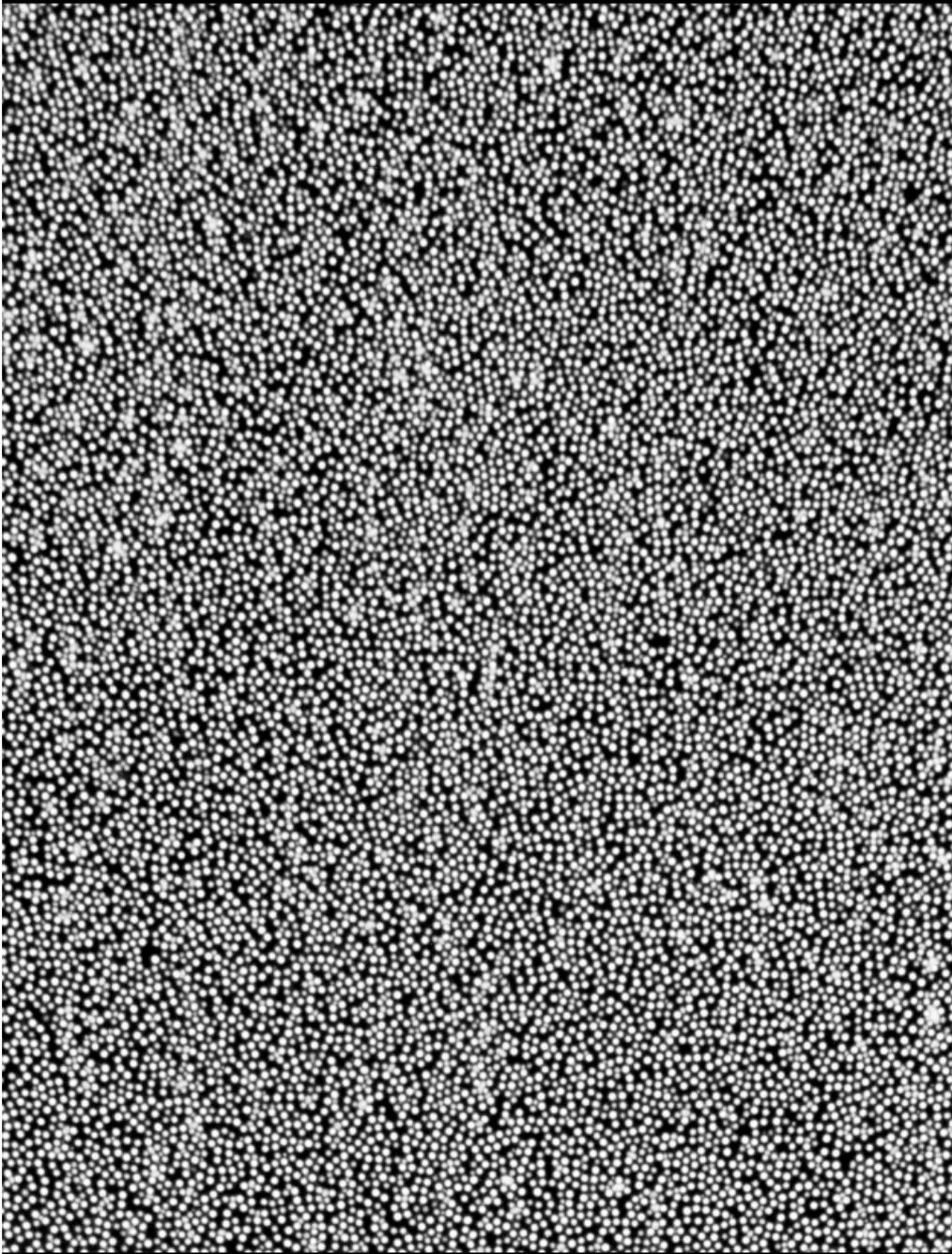
16 h 22 min

Photron

628 x 833

frame : 1

10 x realtime, 5 fps



Fast experiment.

10 times real time, $Ca=0.090$

Fractional flow rate:

$$F=Q_{nw}/Q_{tot}=1/2$$

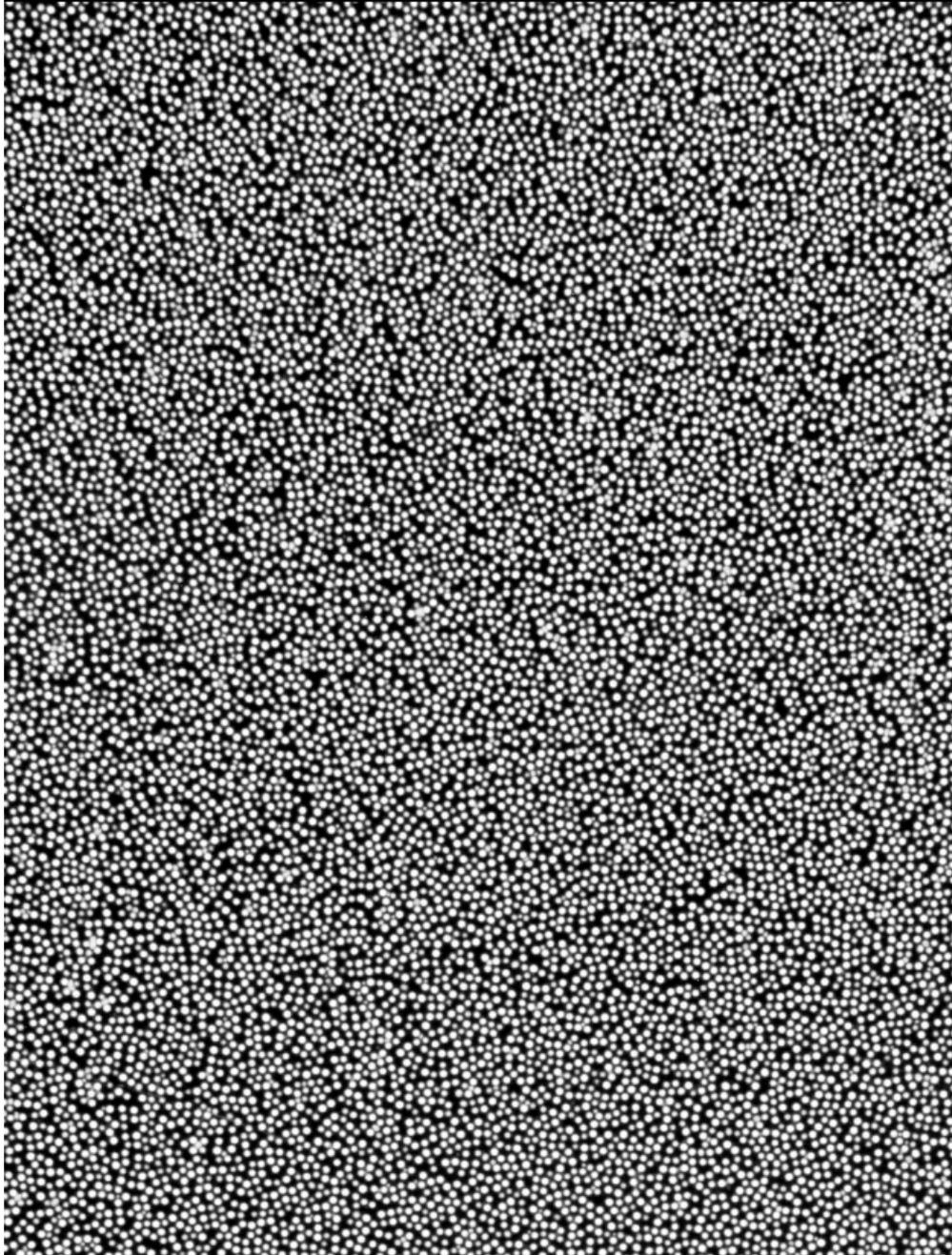
10cm x 15 cm section in the middle
Of the model.

Photron

628 x 837

frame : 1

120 x realtime, 5 f ps



Slow experiment

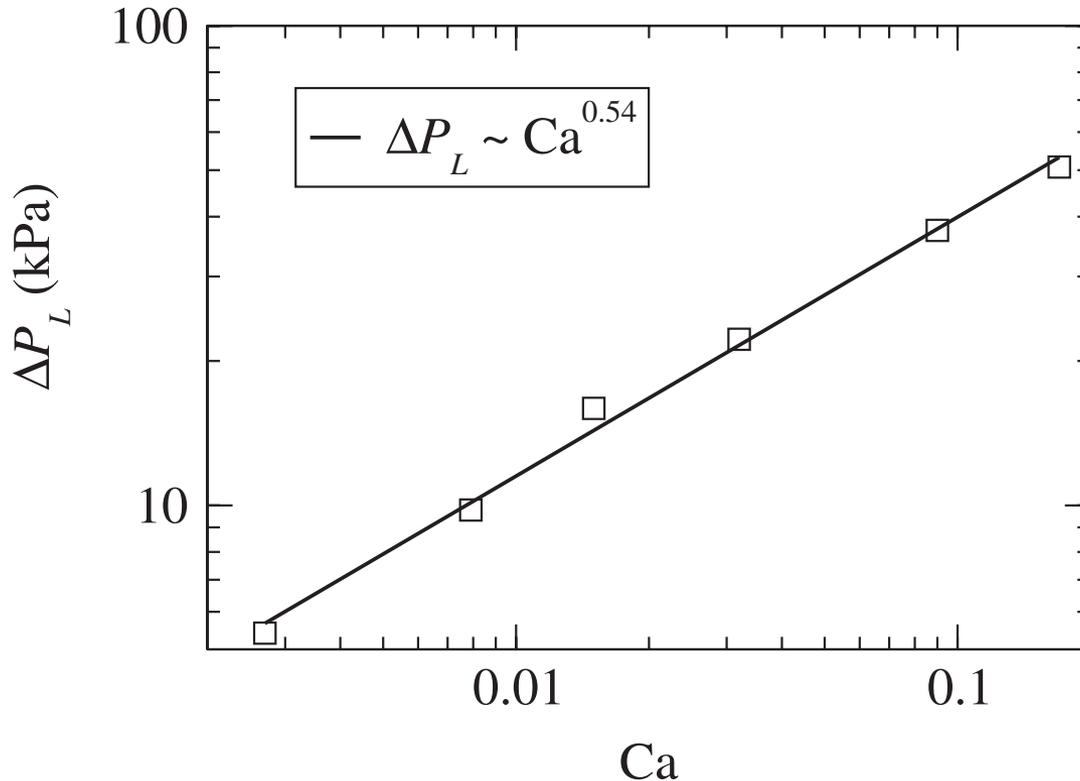
120 times real time, $Ca=0.0079$

10cm x 15 cm section in the middle
Of the model.

Non wetting fluid: Air

Wetting fluid: Water-glycerol

Pressure dependence on capillary number Ca .



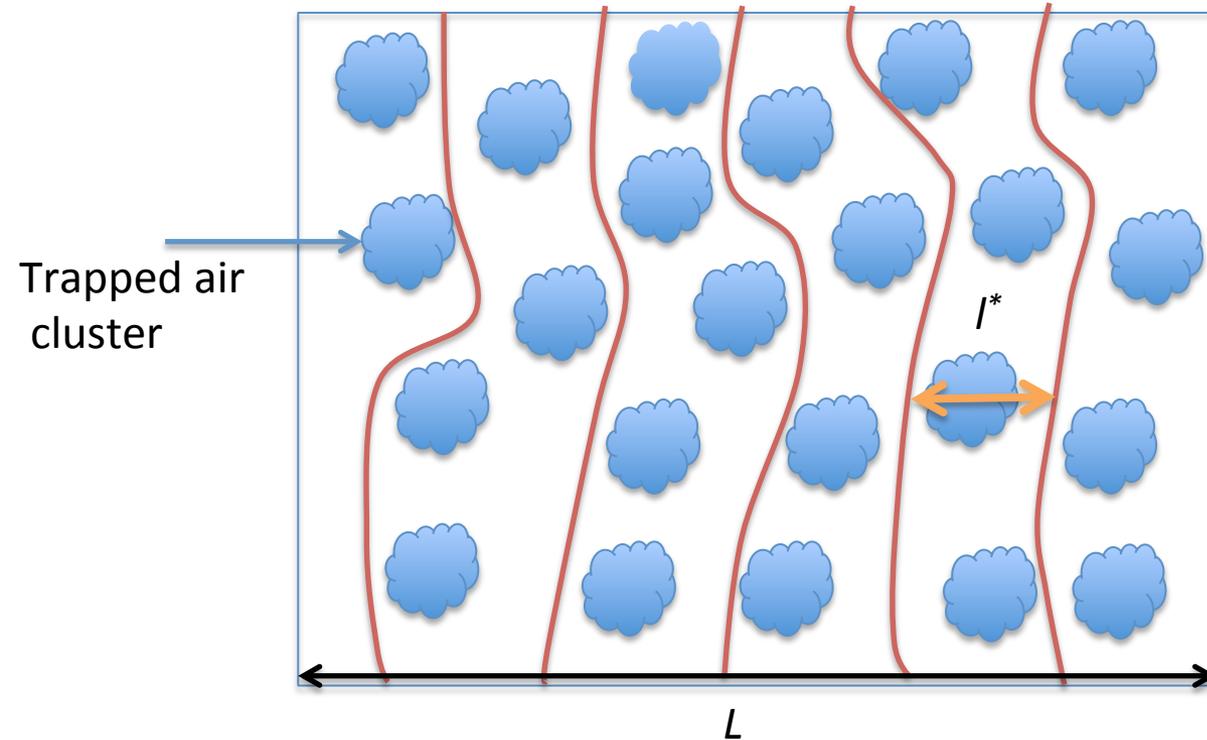
$$Ca = \frac{\mu_w Q_w a^2}{\gamma \kappa_0 A}$$

$$\Delta P \propto Ca^{0.54}$$

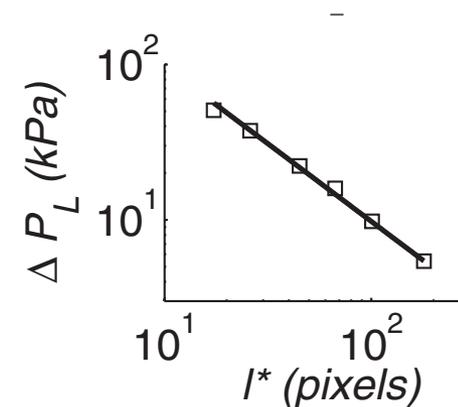
$$\beta = 0.54 \pm 0.08$$

Assumption:

Flow restricted to narrow channels separated a distance corresponding to the characteristic cluster size.



$$N = L/l^*$$



Total flux of wetting fluid:

$$Q = q \cdot N = a^2 \cdot \frac{a^2 \Delta P}{\mu L} \cdot \frac{L}{l^*}$$

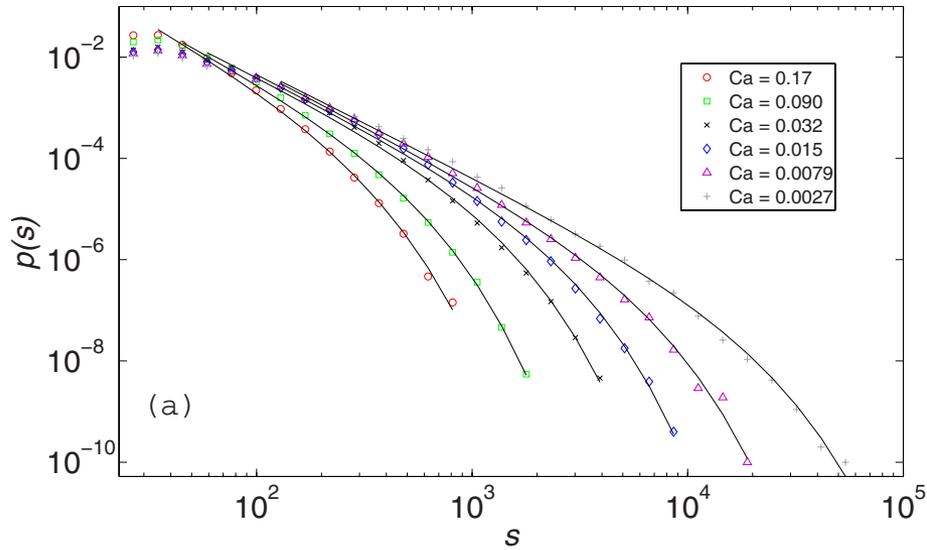
$$\Delta P \propto Q^{1/2} \propto Ca^{1/2}$$

Balance between viscous pressure and capillary threshold.

$$l^* \frac{\Delta P}{L} = \Delta P_c = P_d - P_i$$

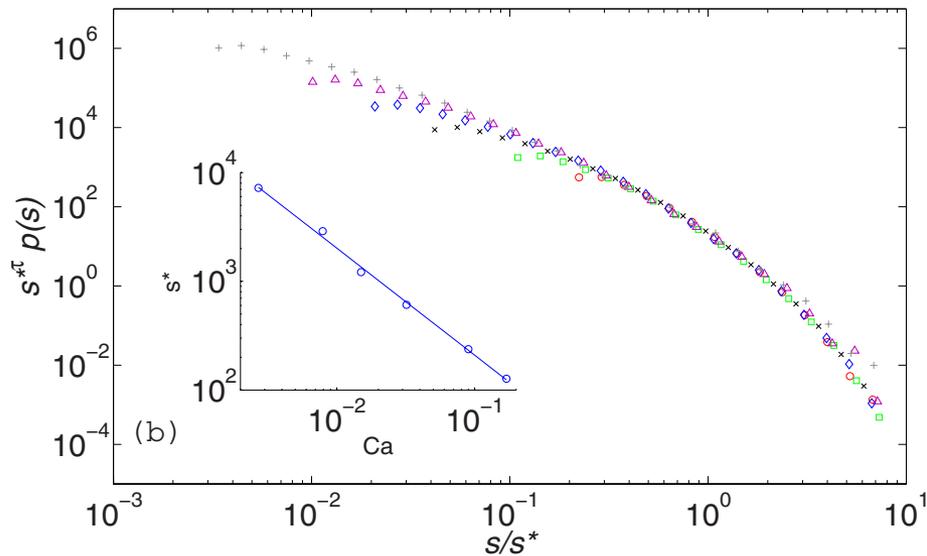
Theory by Eirik G. Flekkøy

Cluster size distribution



$$p(s) \propto s^{-\tau} \exp(-s/s^*),$$

$$\tau = 2.0 \pm 0.2$$

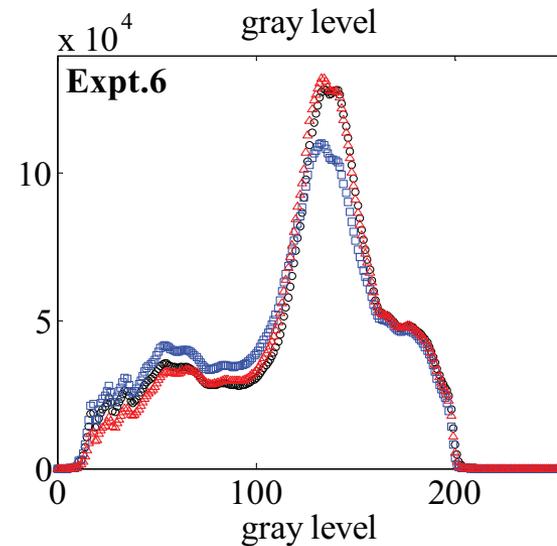
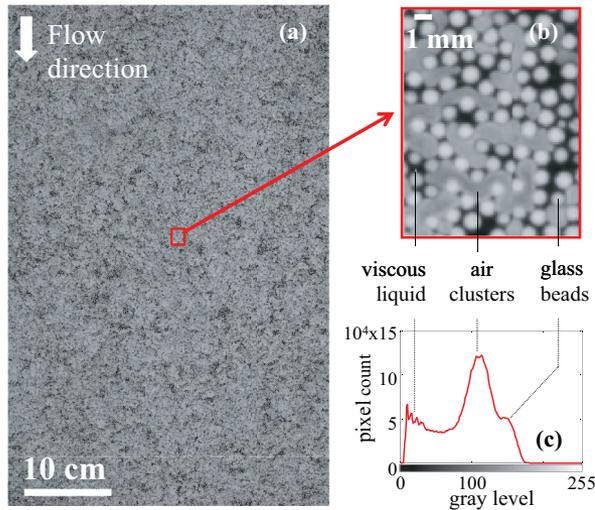
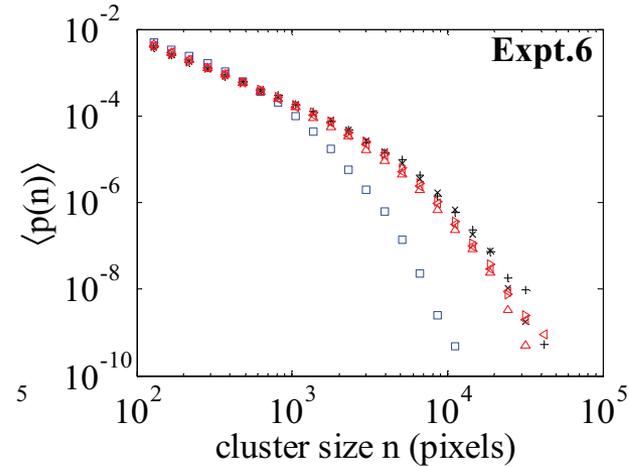
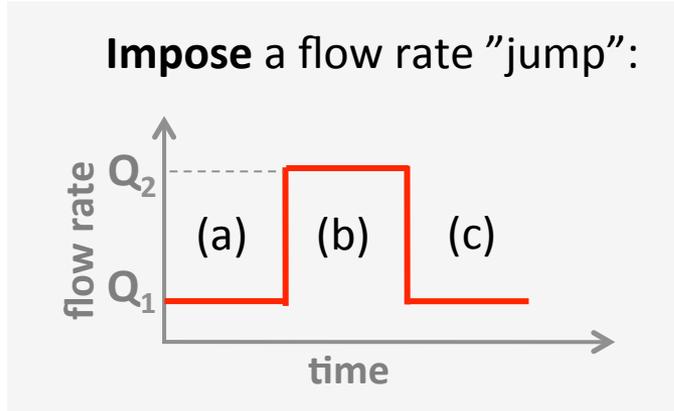


$$s^* \propto Ca^{-\zeta},$$

$$\zeta = 0.98 \pm 0.07.$$

Question: is this "steady state" *really* a state?

i.e., does it depend on the history of the system ?



Case B:

Non wetting fluid: Rapeseed Oil

Wetting fluid: Water-glycerol

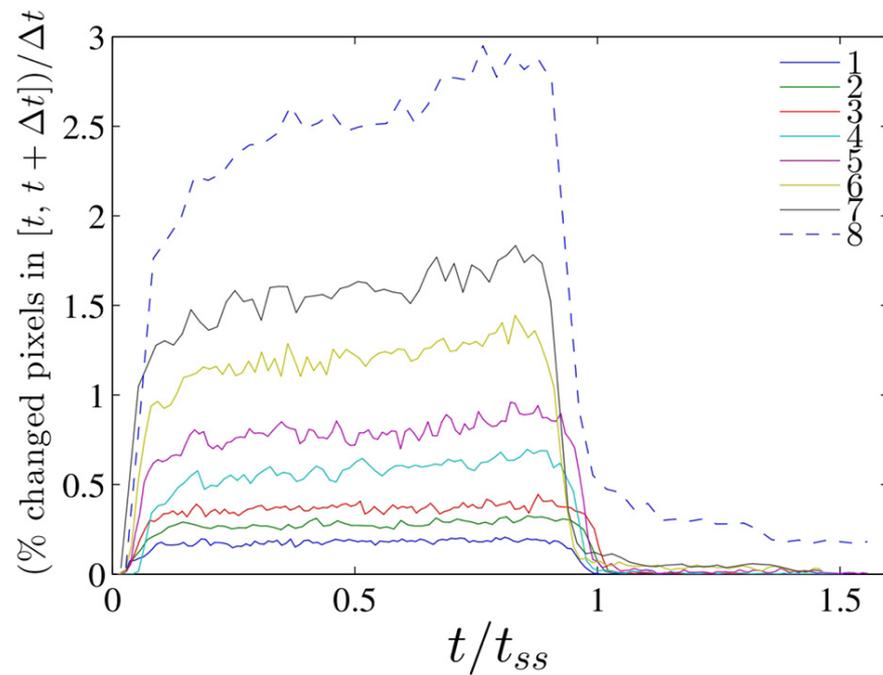
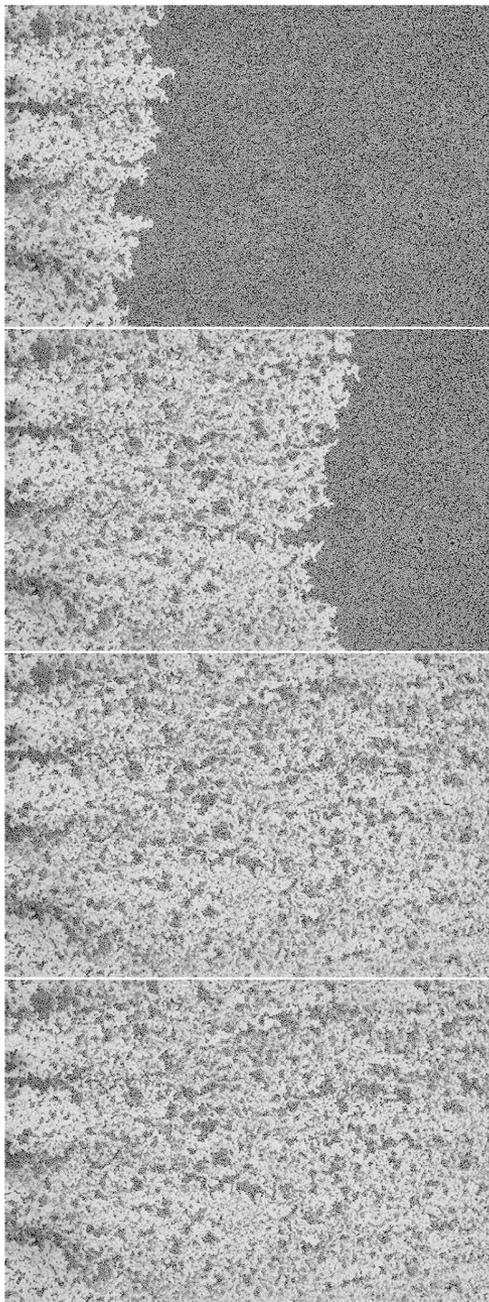


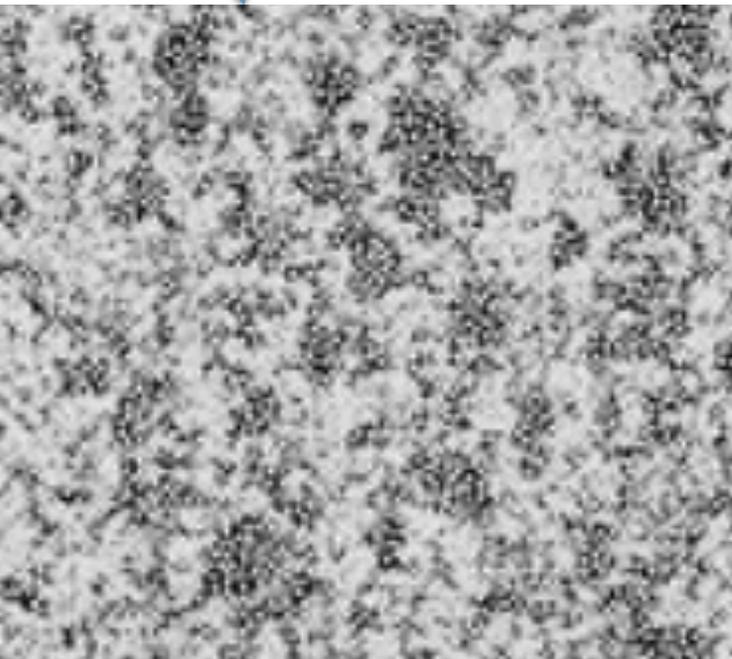
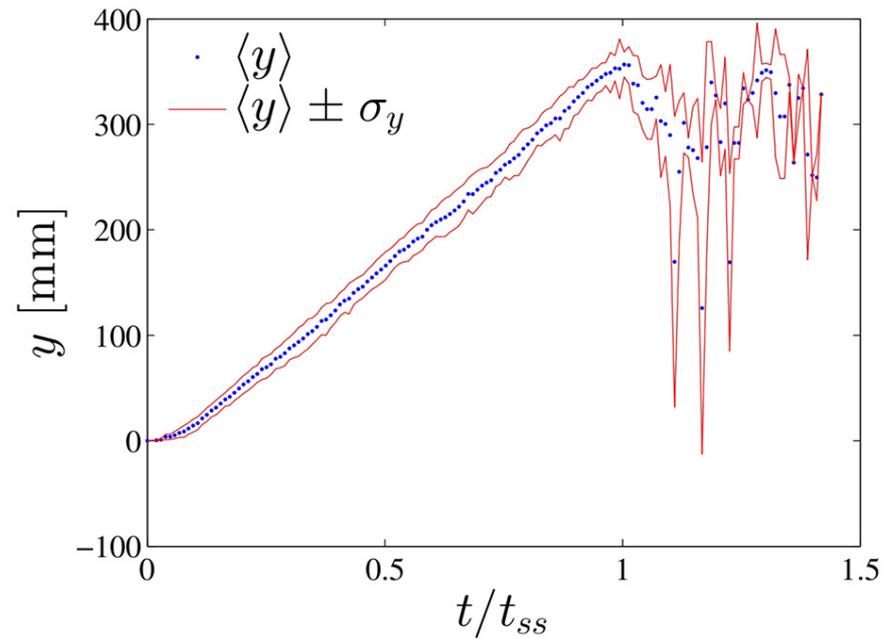
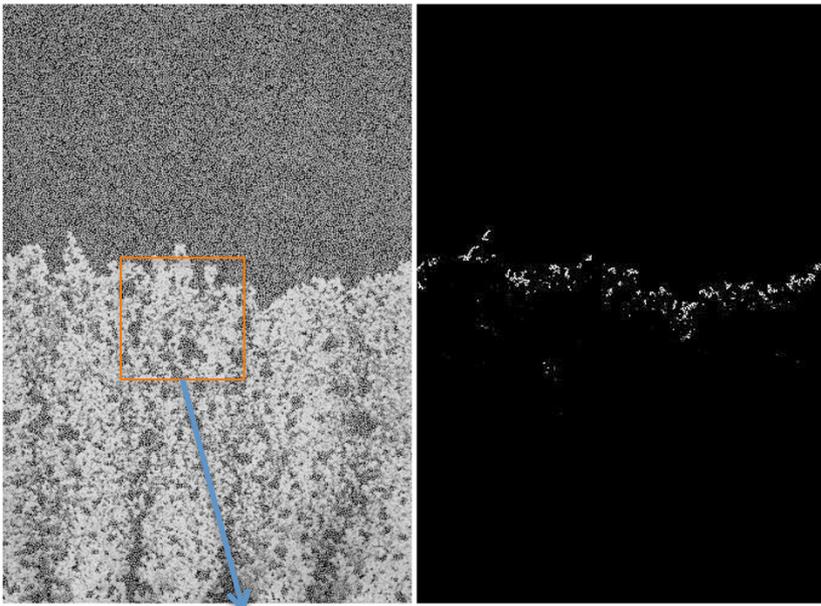
Table 2 | Total flow rates Q_{tot} and capillary numbers Ca corresponding to the legend numbers presented in the forthcoming graphs.

Legend no.	Q_{tot} [ml/min]	Ca
1	0.30	0.0241
2	0.45	0.0362
3	0.60	0.0482
4	0.90	0.0723
5	1.2	0.0964
6	1.8	0.145
7	2.4	0.193
8	3.6	0.289

“Static” cluster configuration

For $Q_{tot} = 0.3$ ml/min and $F_{oil} = 1/2$,

Average position $\langle y \rangle$ of changes as function of time.



“Static” cluster configuration

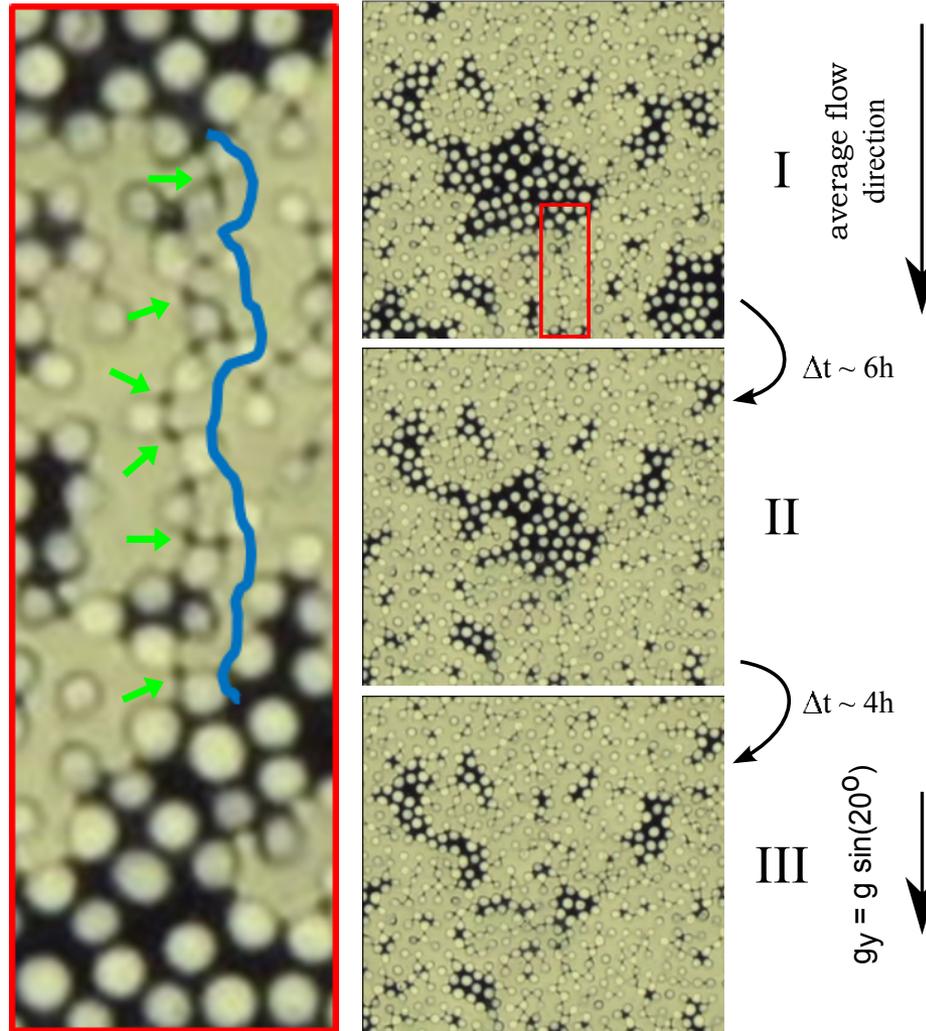
Flow by film or flow trough capillary bridges.

Film flow and capillary bridges

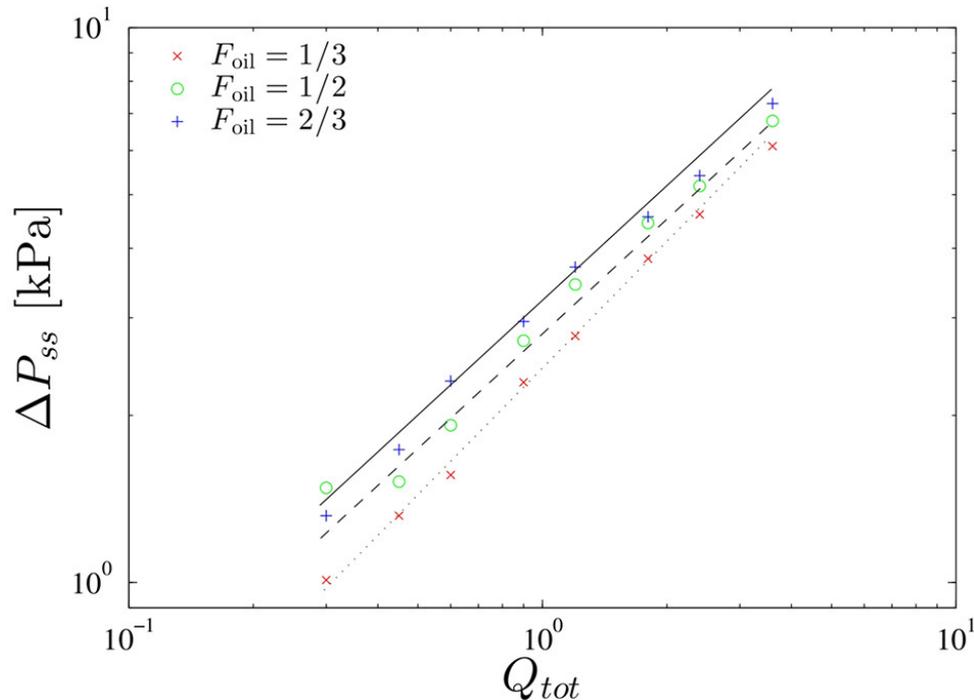
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Experiment by
Marcel Moura

Monem Ayaz



Pressure dependence on capillary number Ca .

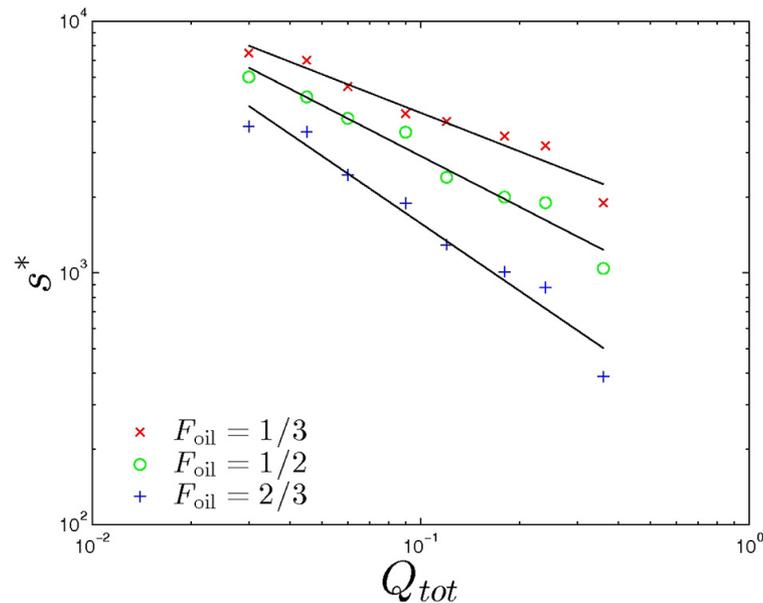
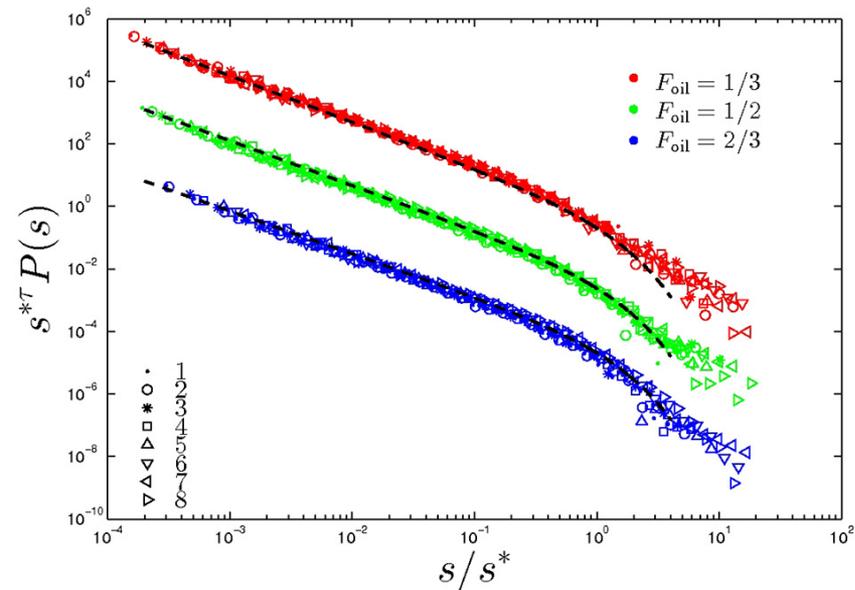


$$\Delta P_{ss} \sim Q_{tot}^{\beta},$$

$\beta_{1/2, 2/3} = 0.67 \pm 0.05$ for $F_{oil} = 1/2$ and $2/3$,

$\beta_{1/3} = 0.74 \pm 0.05$ for $F_{oil} = 1/3$.

Cluster size distribution



$$p(s) \propto s^{-\tau} \exp(-s/s^*),$$

$$\tau_{2/3} = 1.37 \pm 0.09, \quad \tau_{1/2} = 1.43 \pm 0.06,$$

$$\tau_{1/3} = 1.48 \pm 0.04,$$

$$s^* \propto Q_{\text{tot}}^{-\zeta}$$

$$\zeta_{2/3} = 0.89 \pm 0.08, \quad \zeta_{1/2} = 0.67 \pm 0.05,$$

$$\zeta_{1/3} = 0.51 \pm 0.05$$

Summary

<i>Air + water/glycerol</i>	<i>Oil + Water/glycerol</i>
<i>Compressible</i>	<i>Incompressible</i>
$\Delta P_{ss} \sim Q_{tot}^\beta,$ $\beta = 0.54 \pm 0.08$	$\beta = 0.67 \pm 0.05$
$p(s) \propto s^{-\tau} \exp(-s/s^*),$ $\tau = 2.07 \pm 0.18$	$\tau = 1.43 \pm 0.06$
<i>Dynamic air cluster configuration</i>	<i>Static glycerol/water cluster configuration</i>
<i>History independence</i>	?